


# **Ion exchange behavior of ammonium ions on various zeolites**

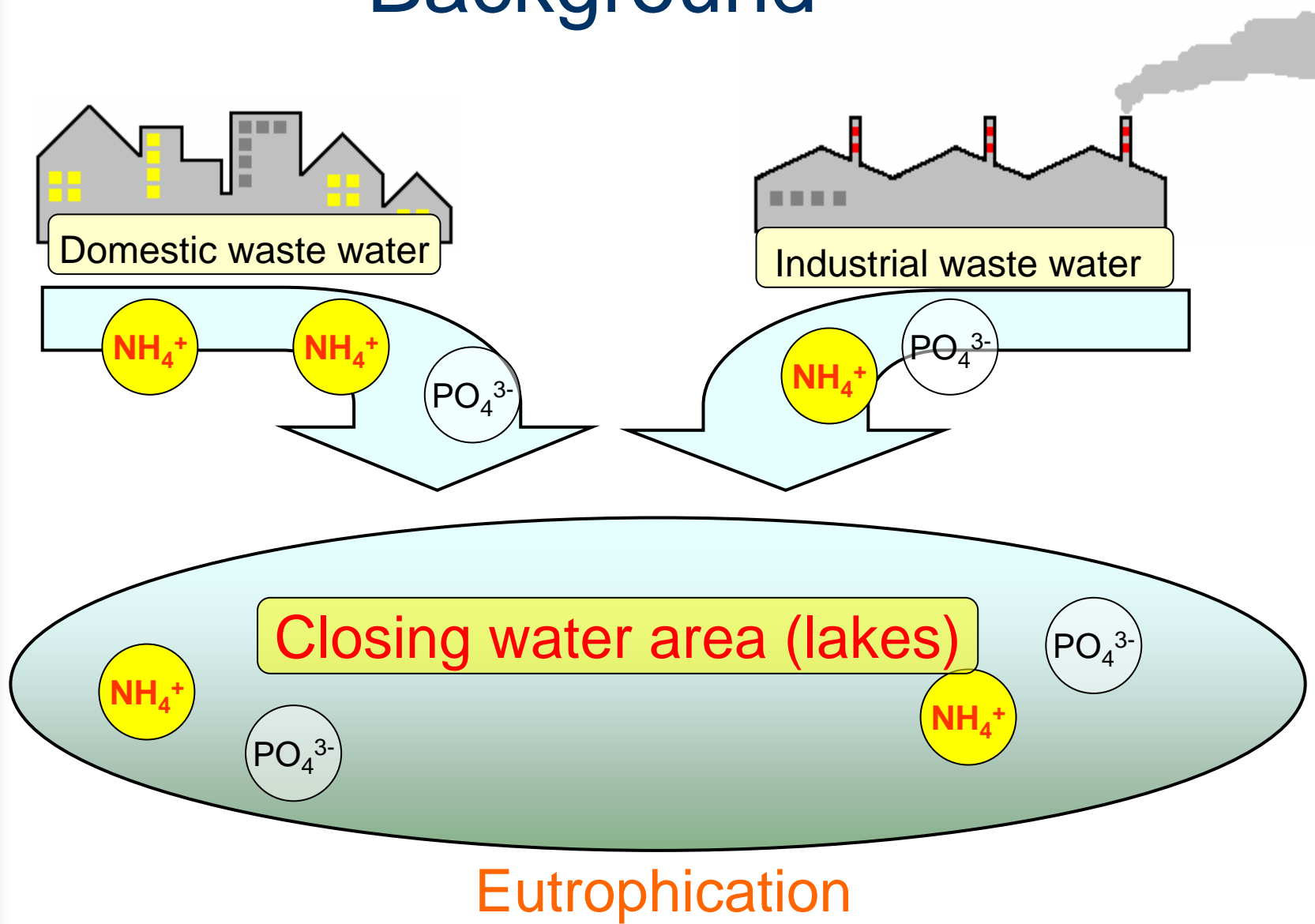


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# Background



# Purpose

Ammonia nitrogen ( $\text{NH}_4^+$ ) is one of main factors of eutrophication in lakes.

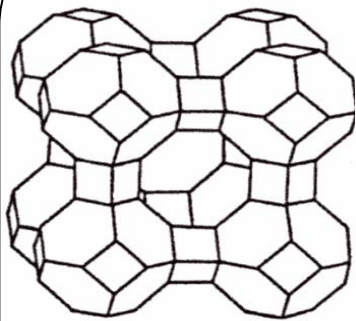
**Zeolites** have been proposed as material for removal of the ammonium ion.

The behavior of  $\text{NH}_4^+$  in ion exchange reaction on different kinds of zeolites, was investigated. In particular the effects of the pH, the reaction time and the concentration of  $\text{NH}_4^+$  in aqueous solutions were examined after those reactions reached to the equilibrium values.

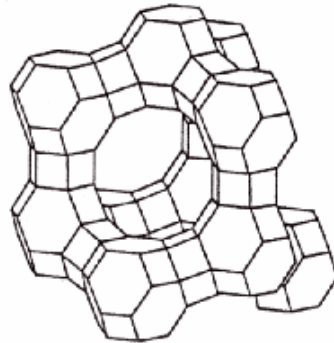
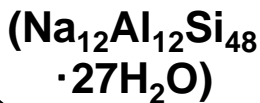
# Materials: Zeolites

## Framework structures

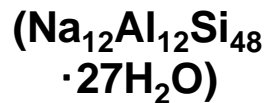
Synthetic zeolites



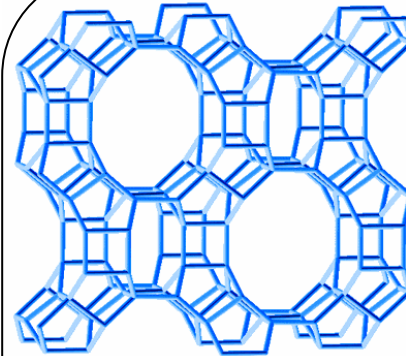
**LTA**



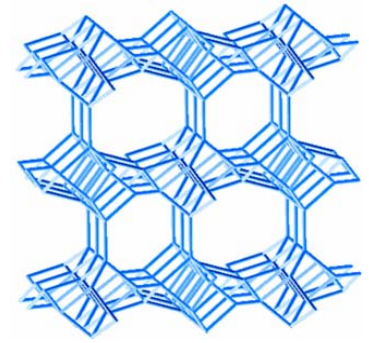
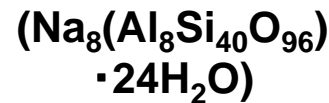
**FAU**



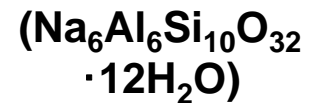
Natural zeolites



**Mordenite**



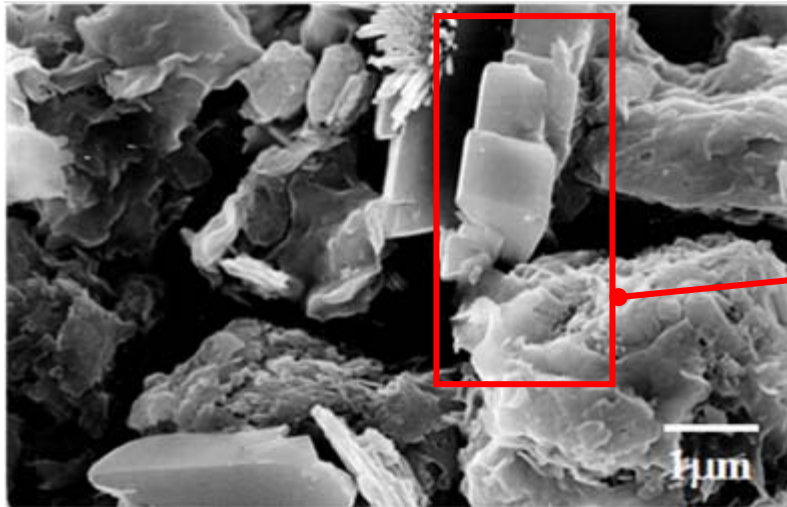
**Clinoptilolite**



## Characteristics

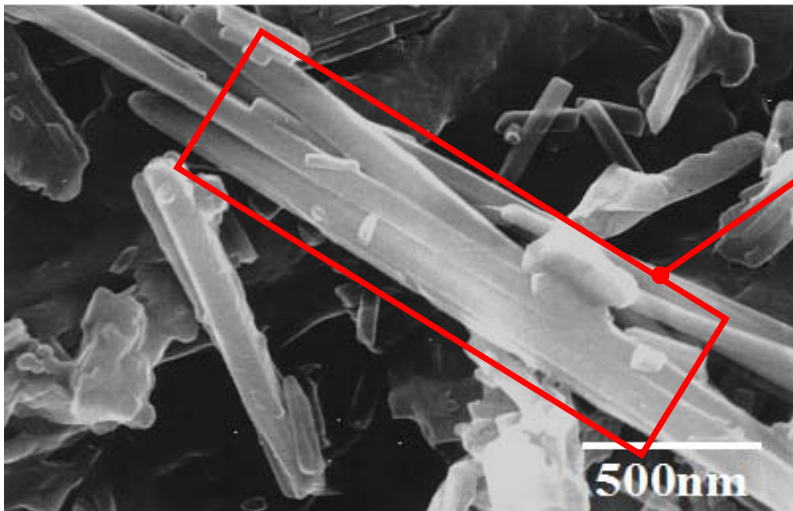
- High cation-exchange capacity  
(**High ammonium ion-selectivity**)
- Ion adsorption

# Observation for Zeolites by SEM (1)



Natural zeolites  
(Shimane prefecture, Japan)

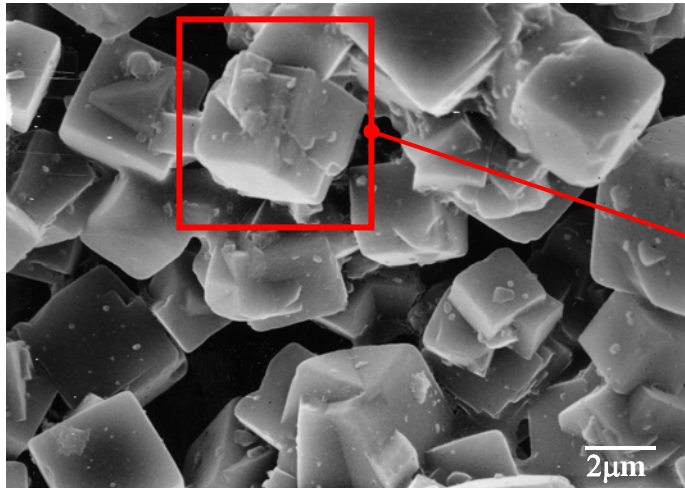
Clinoptilolite is coffin-shape crystals and submicron in size.



Mordenite is fibrous and ranged from 0.05 to 0.1 mm in diameter and from 1 to 5 mm in length.

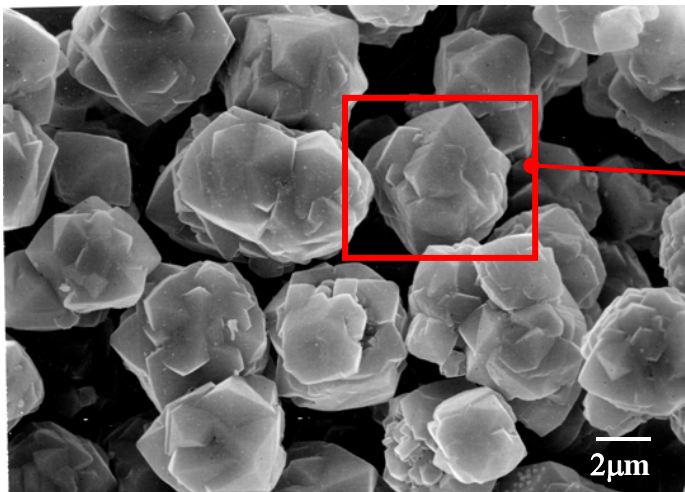
**Fig. SEM images of clinoptilolite and mordenite in natural zeolite from Shimane, Japan.** *Y.Watanabe et al. Sep.Sci.Tech.(2003).*

# Observation for Zeolites by SEM (2)



Synthetic zeolites  
(LTA, FAU)

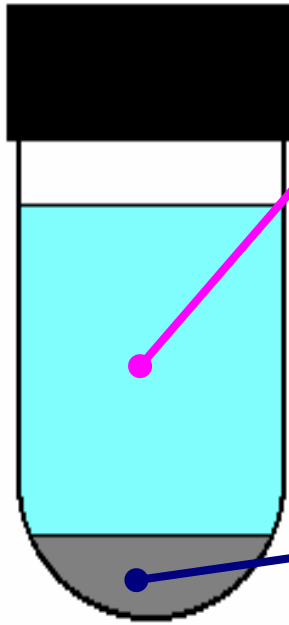
• LTA is intergrowth of typical cubic crystallites of micron size in diameter



• FAU is aggregate or intergrowth of fine octahedral crystallites of submicron size in diameter

Fig. SEM images of LTA and FAU. *Y.Watanabe et al. Sep.Sci.Tech.(2003).*

# Experimental procedure



**Ammonium chloride solution:**  $30\text{cm}^3(1.0 \times 10^{-3}\text{mol dm}^{-3})$

**Time dependence:** Reaction time: 1~168hrs, pH: 2.0~2.3

**pH dependence:** pH: 1~6(Hydrochloric acid)

Reaction time: 24hrs, 168hrs

**Dependence of Ammonium ion concentration:**

Concentration:  $1.0 \times 10^{-4} \sim 3.0 \times 10^{-3}\text{mol dm}^{-3}$

**Synthetic zeolites :** LTA(3A)、FAU(13X)

**Natural zeolites :** Indonesia A 、 Indonesia B、

Shimane 、 Australia

: 0.1g (200~250mesh)

**centrifugation (1500rpm)**

**filtration ( $0.45 \mu\text{m}$ )**

**Liquid phase:** FIA (flow injection analyzer)、 ICP-AES

**Solid phase:** SEM

# Calculation of the amount of ammonium-ion capture in percent

**The amount of ammonium-ion capture (%)** = 
$$\frac{C_0 - C_1}{C_0} \times 100$$

$C_0$  : Initial concentration (mmol dm<sup>-3</sup>)

$C_1$  : Equilibrium concentration (mmol dm<sup>-3</sup>)



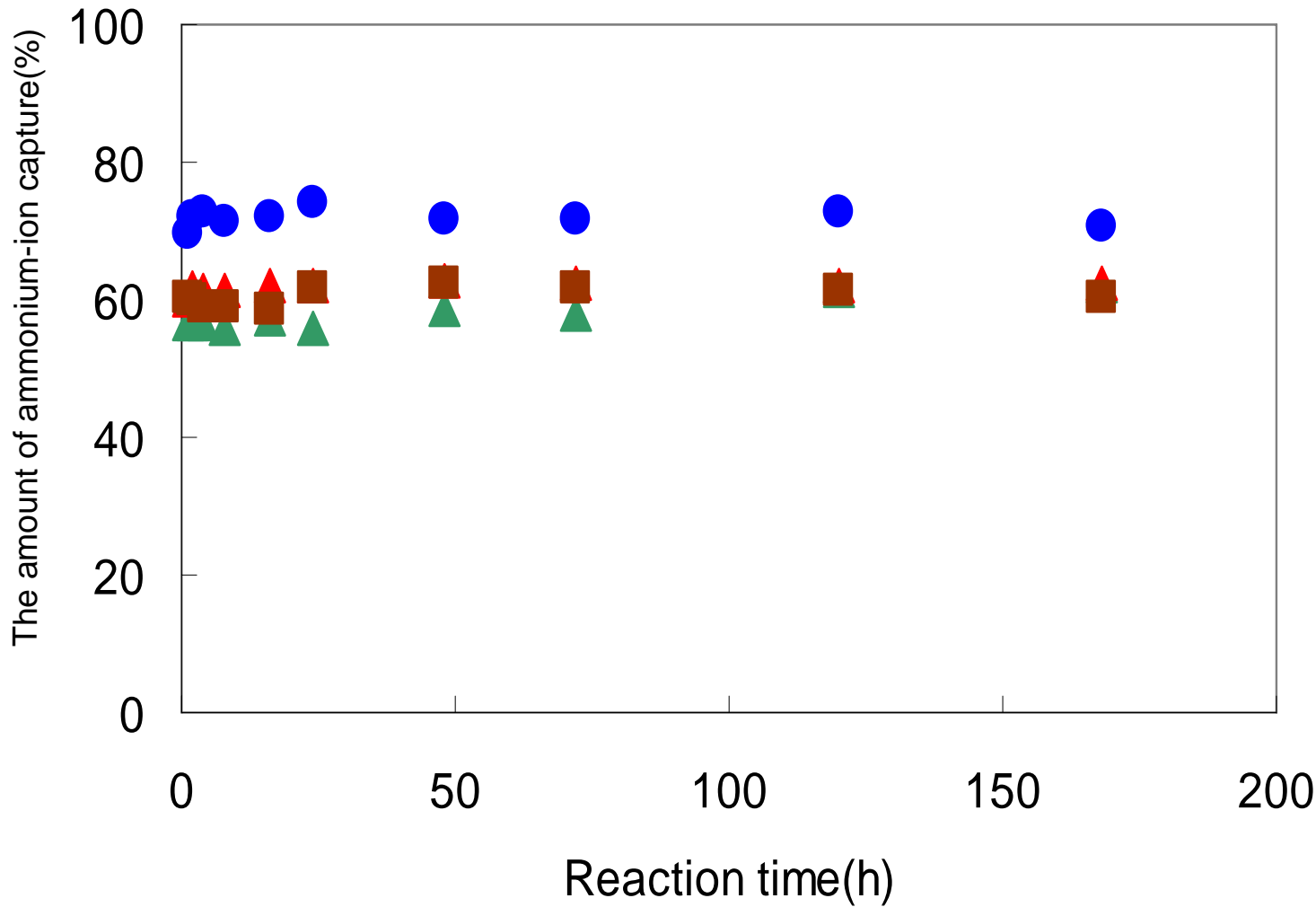


Fig. Relationship between the amount of ammonium-ion capture and the reaction time

● : FAU(X)    ▲ : LTA    ■ : Shimane    ▲ : Indonesia B

Reaction time : 1 ~ 168hrs

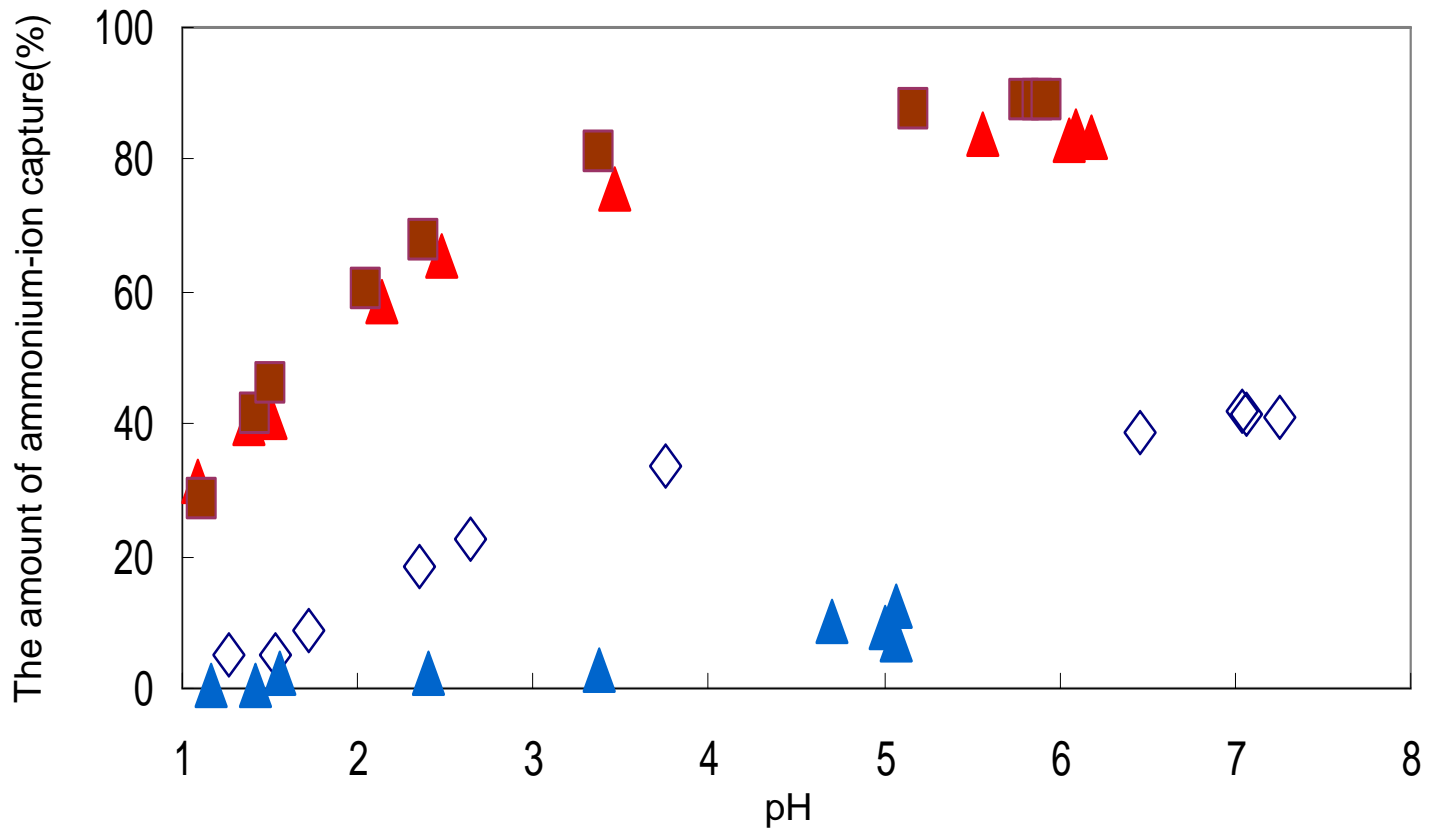


Fig. Relationship between the amount of ammonium-ion capture in percent and the pH in the aqueous solution after reaction.

◇ : Australia      ▲ : Indonesia A

▲ : Indonesia B      ■ : Shimane

Reaction time : 24hrs

# Results and Discussion

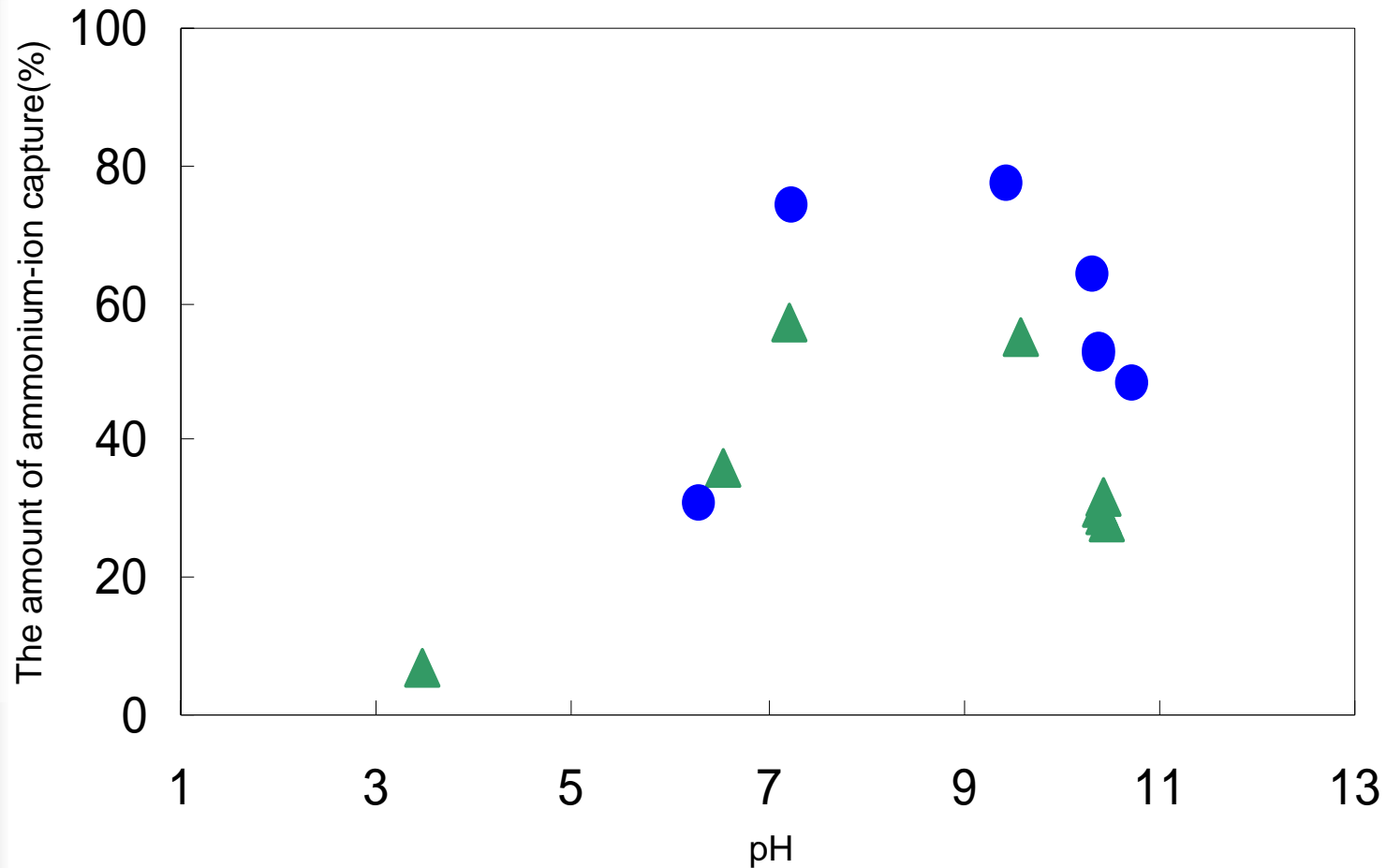


Fig. Relationship between the pH and the amount of ammonium-ion capture on synthetic zeolites.

● :FAU (X), ▲ :LTA .

Reaction time : 24hrs.

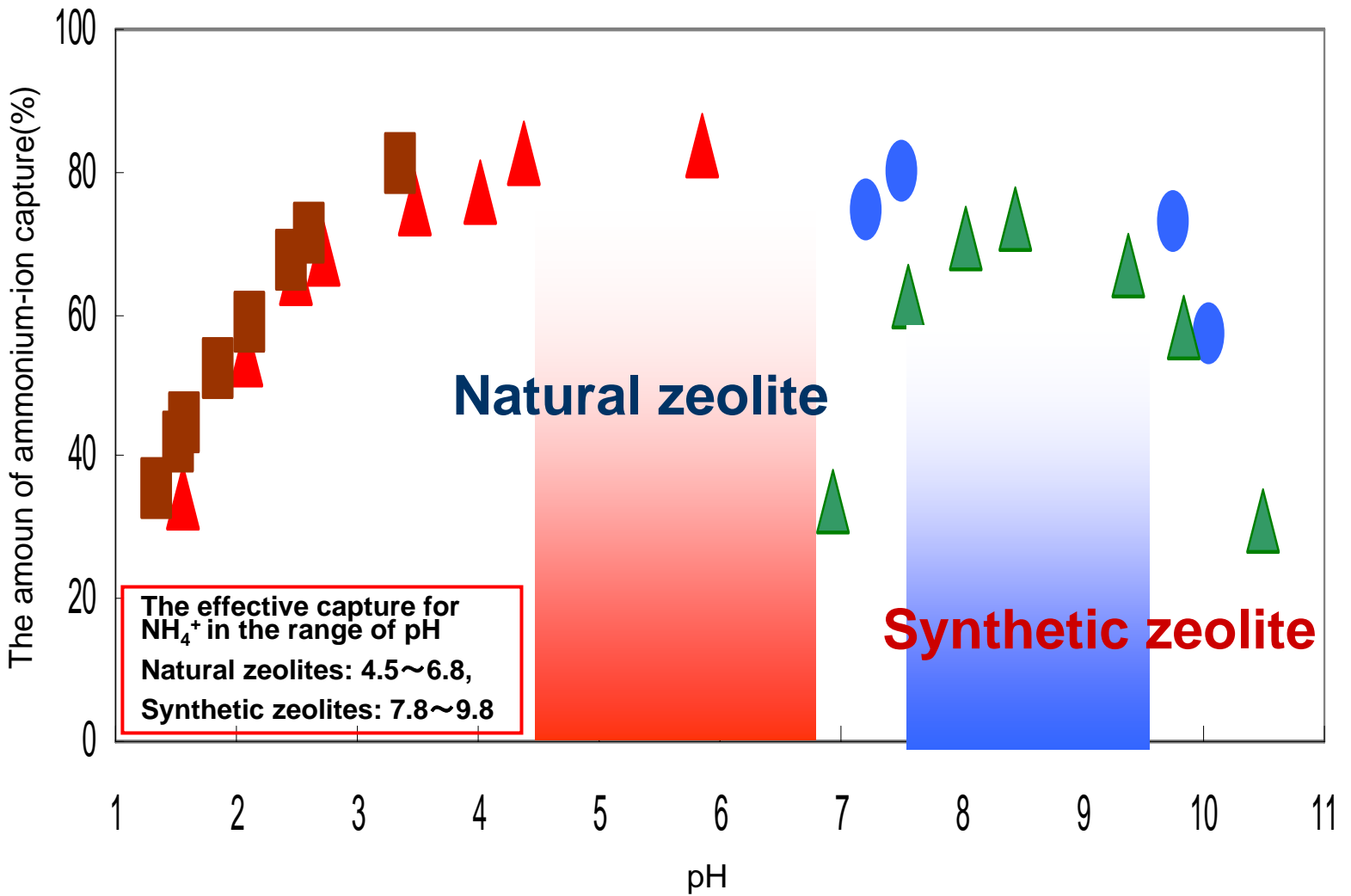


Fig. Relationship between the amount of ammonium-ion capture and the pH.

FAU : ● LTA : ▲ Shimane : ■ Indonesia B : ▲  
 Reaction time: 168hrs

# Ammonium ion exchange behavior

Table. Ammonium ion exchange behavior of zeolite

	$C_0(\text{NH}_4^+)$	$\text{pH}_0$	$\text{pH}_{\text{eq}}$	$\text{SiO}_2$	$\text{Al}_2\text{O}_3$	$\text{Na}^+$	$\text{K}^+$	$\text{Ca}^{2+}$	$\text{Mg}^{2+}$	$C_1(\text{NH}_4^+_{\text{cal}})$	$C_2(\text{NH}_4^+_{\text{exp}})$
MOR	3.0	5.42	5.59	0.017	0.000	1.340	0.143	0.086	0.063	0.514	0.568
	1.0	5.30	6.02	0.018	0.000	0.700	0.050	0.021	0.022	0.231	0.270
	0.3	5.52	6.17	0.024	0.001	0.210	0.018	0.004	0.002	0.051	0.084
	0.1	5.70	6.43	0.023	0.001	0.130	0.014	0.009	0.003	0.029	0.027

MOR: mordenite zeolite

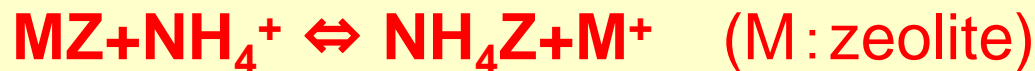
$C_0(\text{NH}_4^+)$ : initial concentration ( $\text{mmol dm}^{-3}$ ),  $\text{pH}_0$ : initial pH,  
 $\text{pH}_{\text{eq}}$ : equilibrium pH,

$C_1(\text{NH}_4^+_{\text{cal}})$ : The theoretical values for ammonium ion exchange quantity  
 ( $\text{mmol/g}$ )

$$[\text{NH}_4^+_{\text{cal}} (\text{mmol dm}^{-3})] = [\text{Na}^+ (\text{mmol dm}^{-3})] + [\text{K}^+ (\text{mmol dm}^{-3})] + \\
 1/2[\text{Mg}^{2+} (\text{mmol dm}^{-3})] + 1/2[\text{Ca}^{2+} (\text{mmol dm}^{-3})]$$

$C_2(\text{NH}_4^+_{\text{exp}})$ : The experimental values for ammonium ion exchange  
 quantity

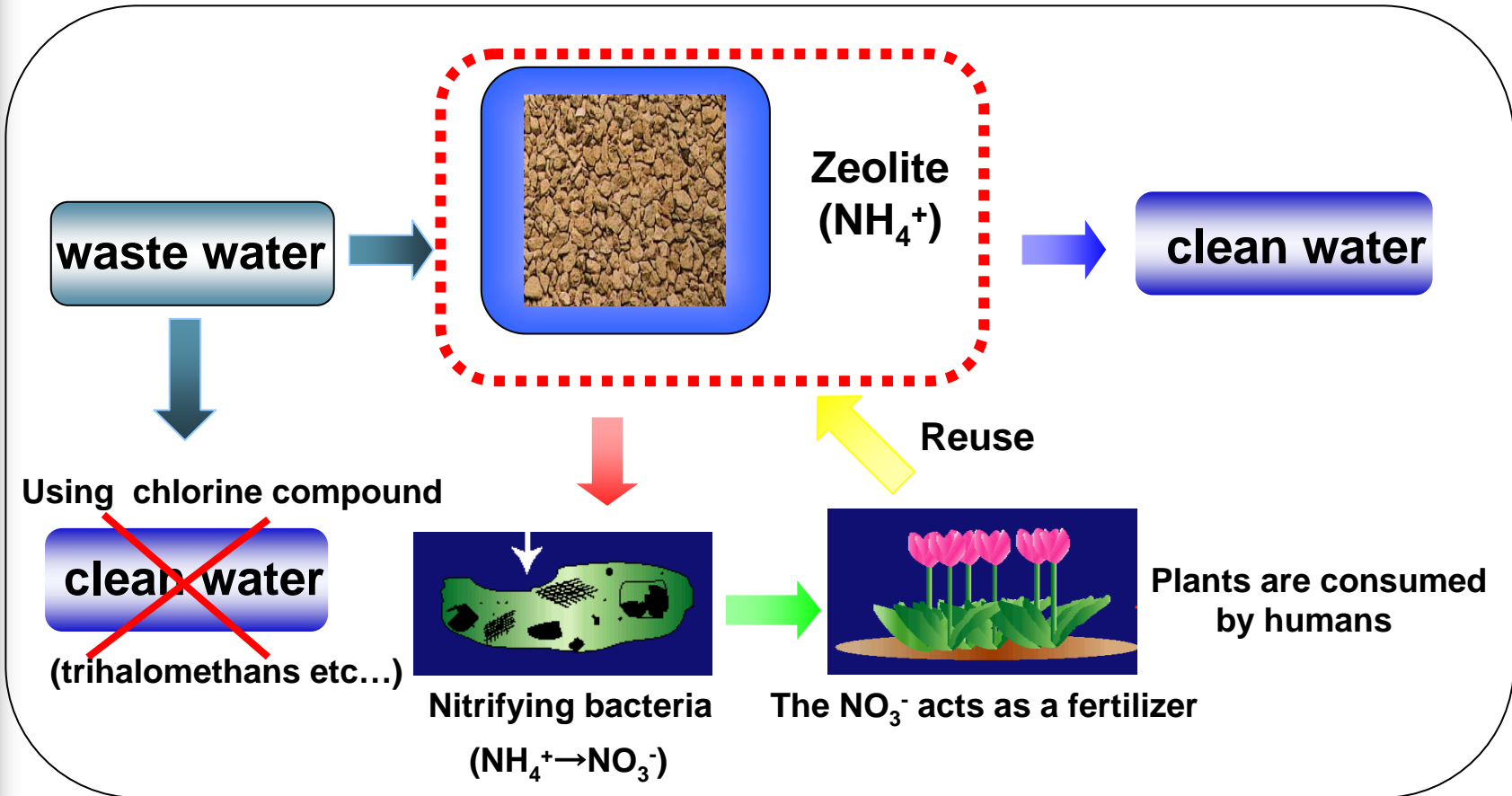
$$C_1(\text{NH}_4^+_{\text{cal}}) \doteq C_2(\text{NH}_4^+_{\text{exp}})$$



# Summary

- The natural zeolites which we used are available to catch the high concentration of  $\text{NH}_4^+$  ions in the range of pH 4.5~6.8, because the average values in the lake are pH 4.5~5.5 in Japan,.
- The reaction for  $\text{NH}_4^+$  capture on natural zeolites reached to equilibrium within 10 min. These fast reaction is very useful for a clean water system.
- The experimental values ( $C_2:\text{NH}_4^+\text{exp}$ ) are closed to theoretical values ( $C_1:\text{NH}_4^+\text{cal}$ ).
- These reactions can be written in the following equation;  
 **$\text{MZ} + \text{NH}_4^+ \rightleftharpoons \text{NH}_4\text{Z} + \text{M}^+$**  (M: zeolite)

# Application



To use zeolite for ammonium ion removal from waste water system